

# THE PSYCHROMETRIC CHART: Theory and Application

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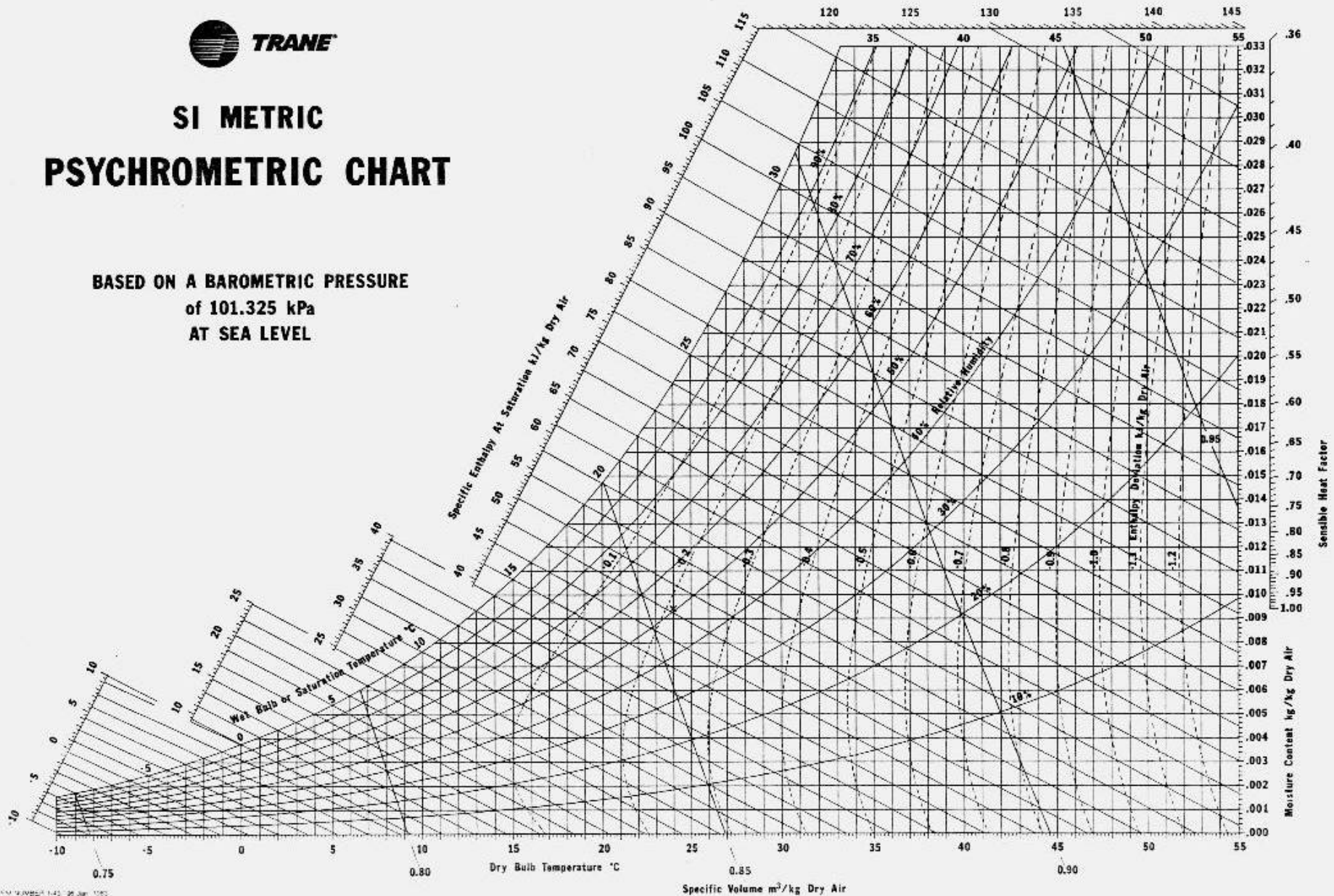
# PSYCHROMETRIC CHART

- Identify parts of the chart
- Determine moist air properties
- Use chart to analyze processes involving moist air



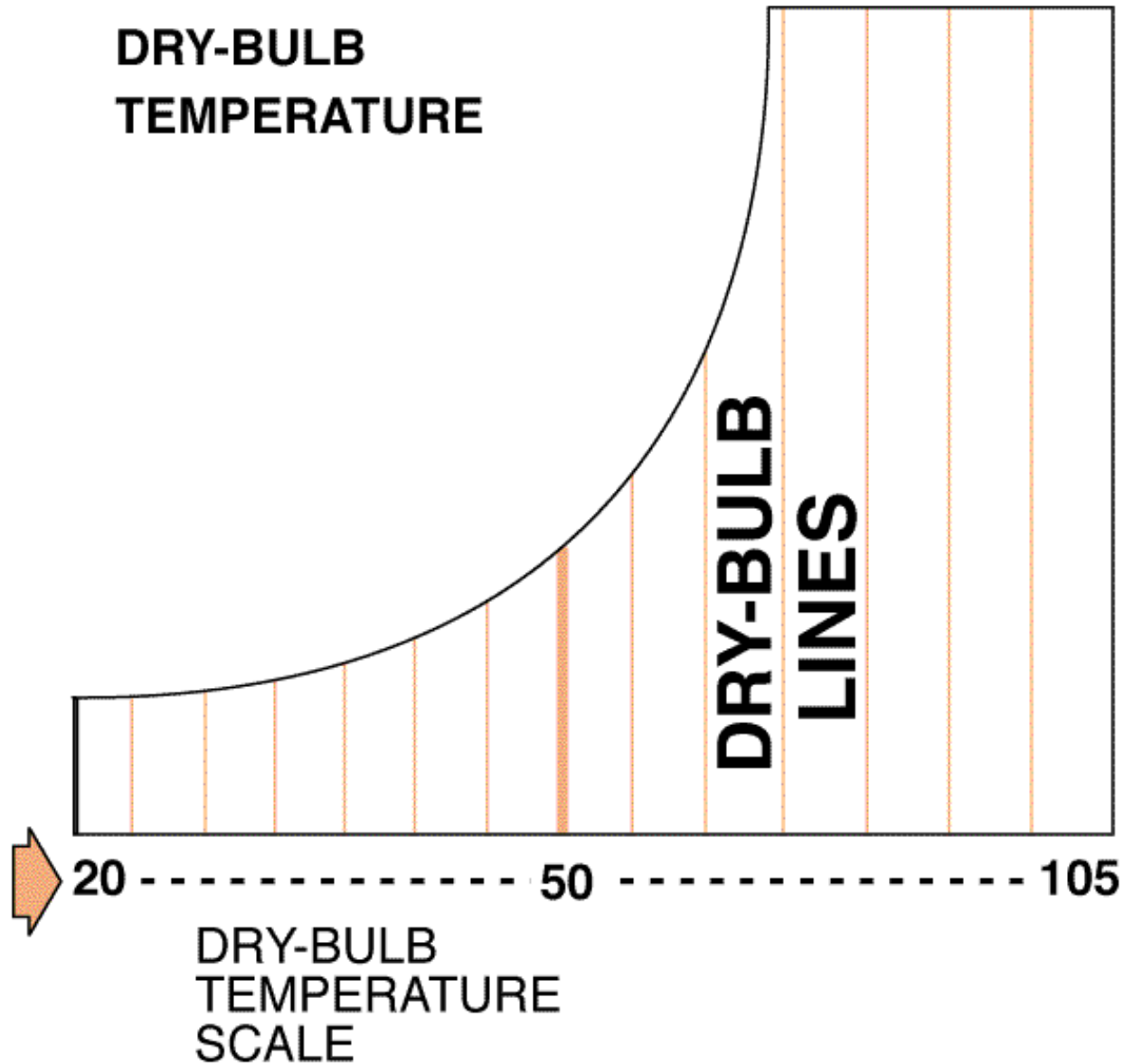
# SI METRIC PSYCHROMETRIC CHART

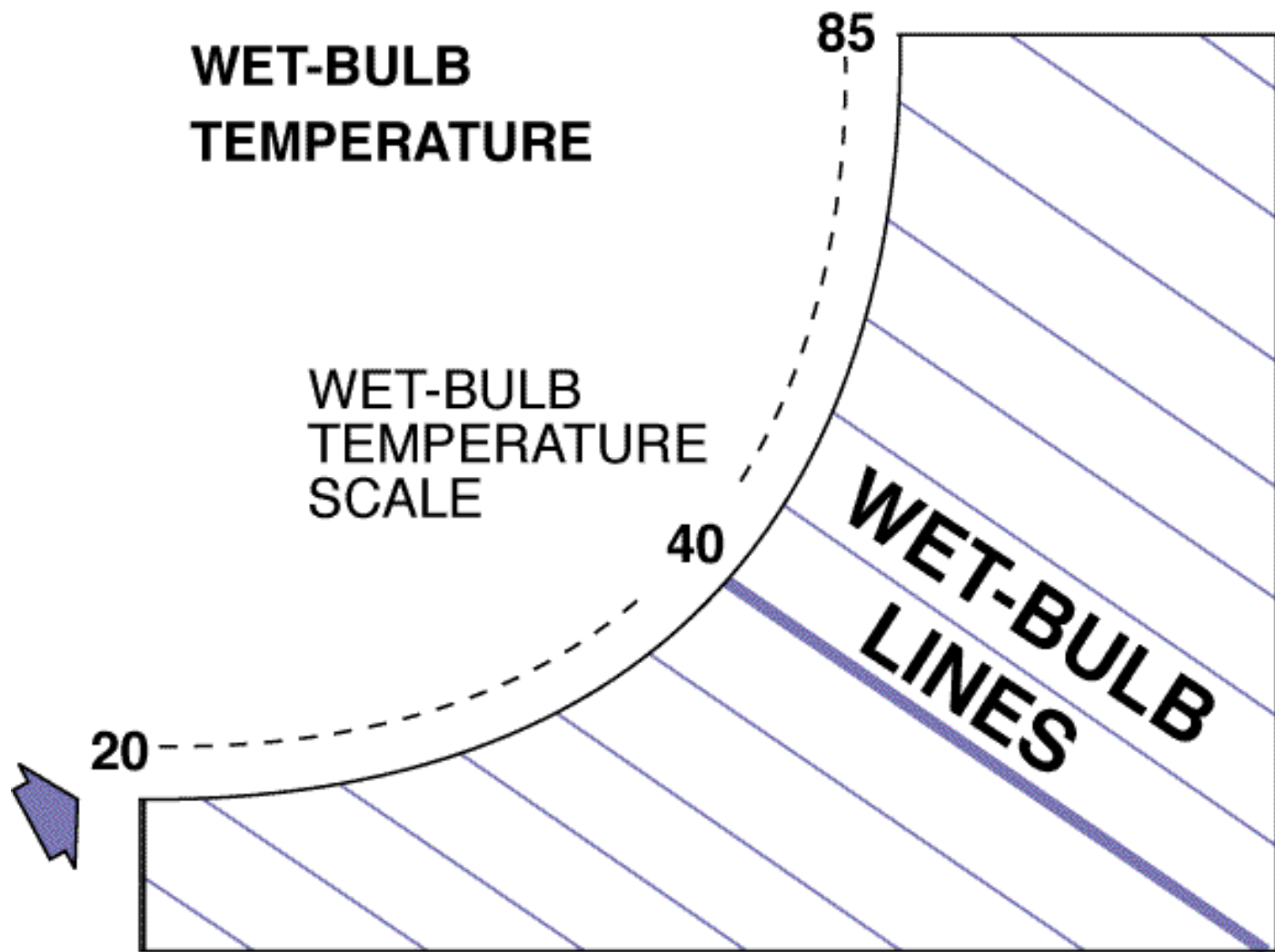
BASED ON A BAROMETRIC PRESSURE  
of 101.325 kPa  
AT SEA LEVEL



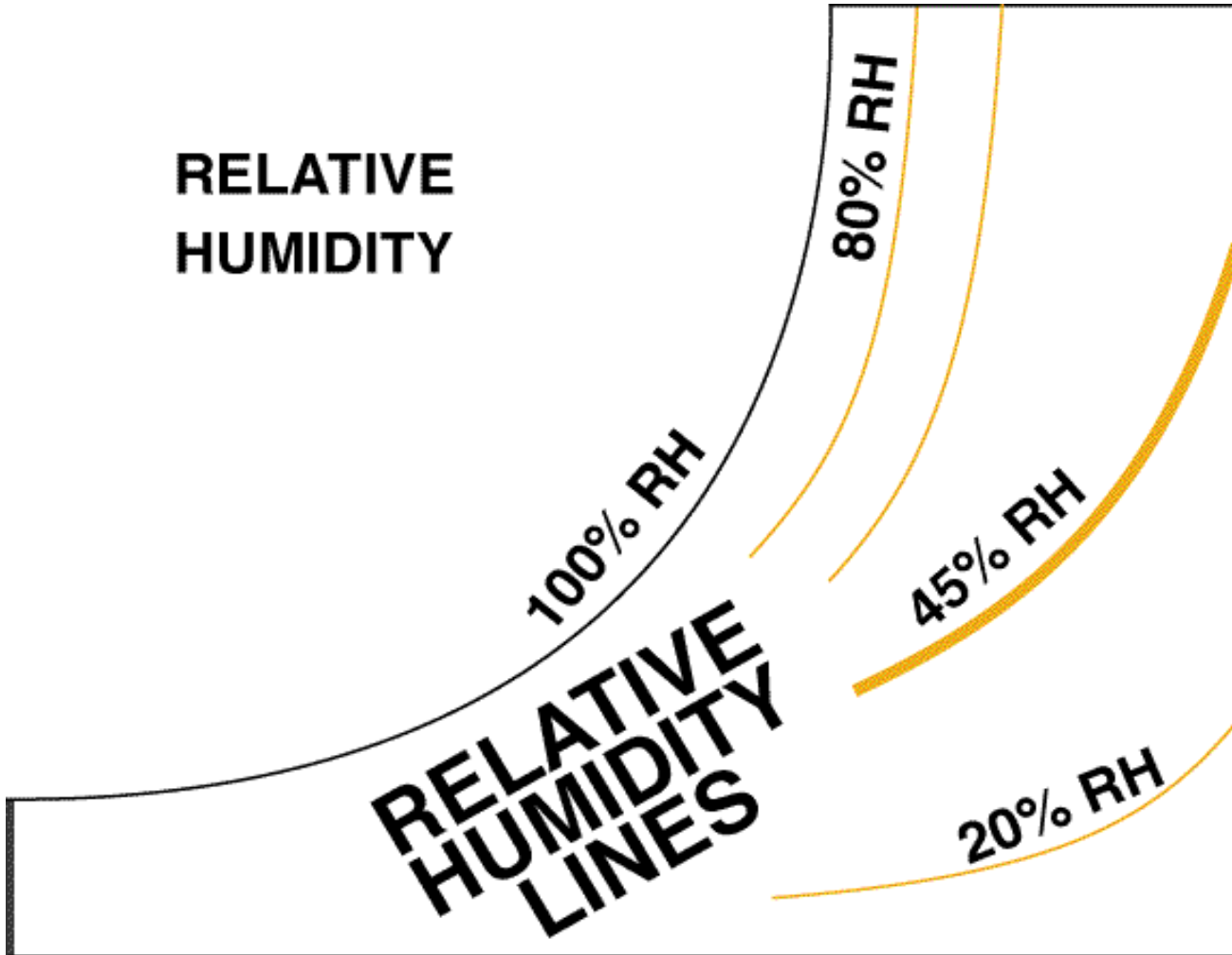
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**DRY-BULB  
TEMPERATURE**





**RELATIVE  
HUMIDITY**

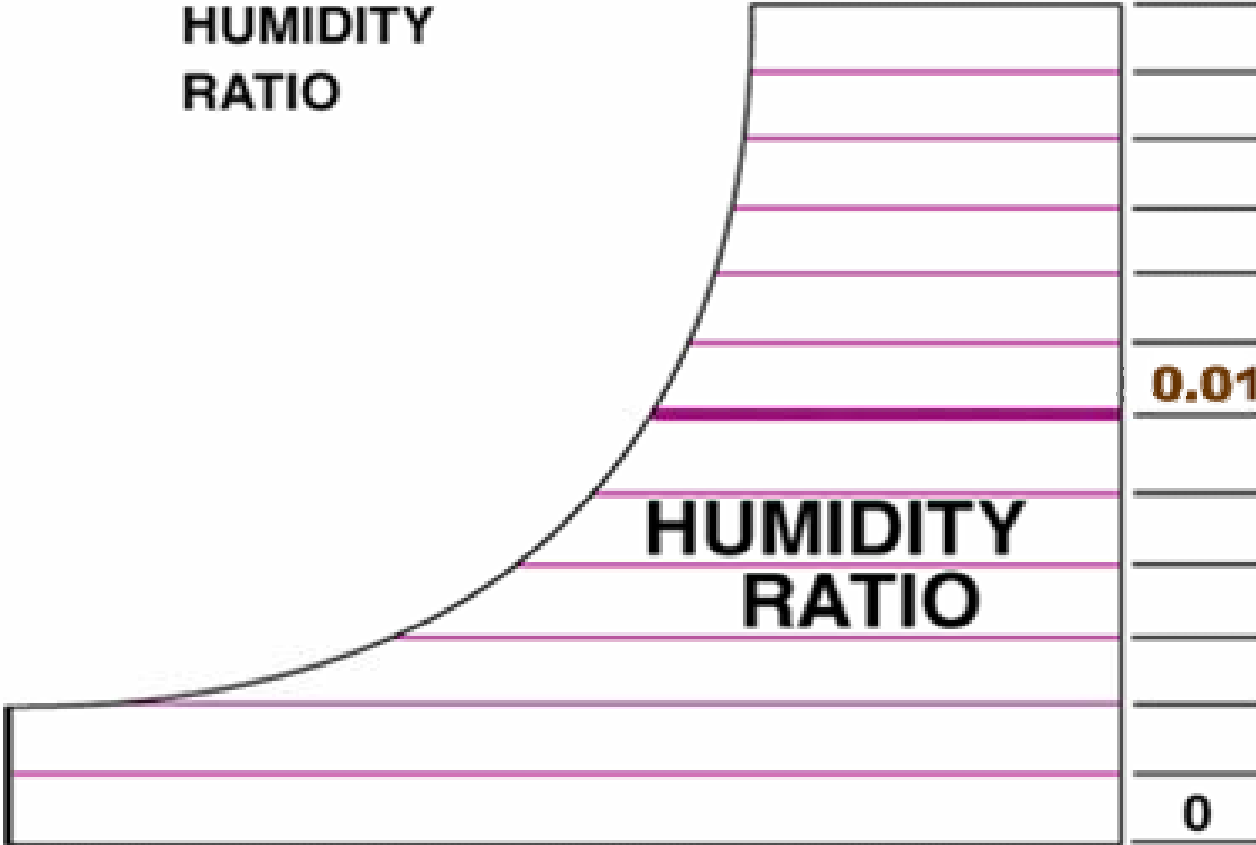


**Kg of moisture  
per kg of dry air**



**0.02**

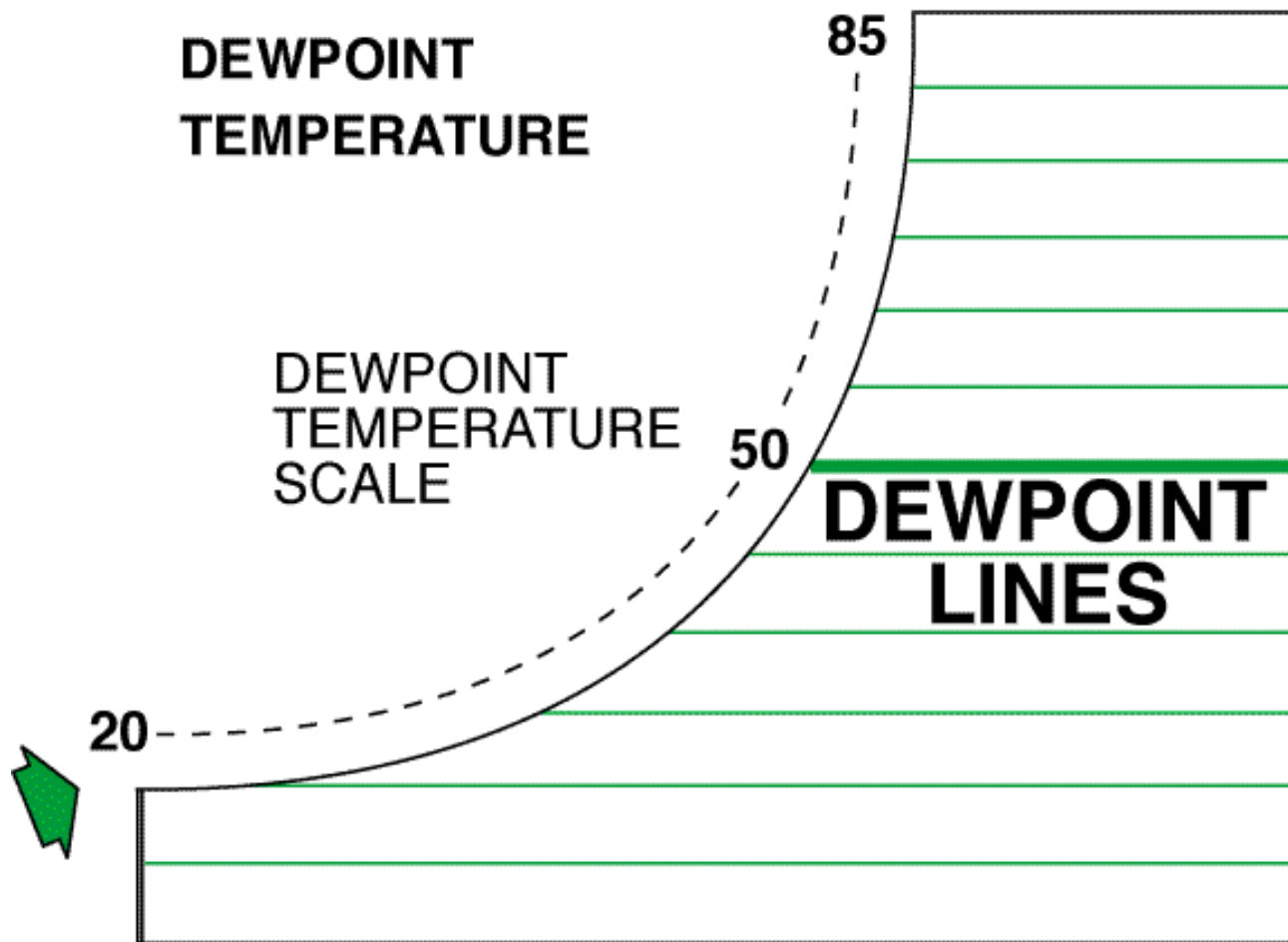
**HUMIDITY  
RATIO**



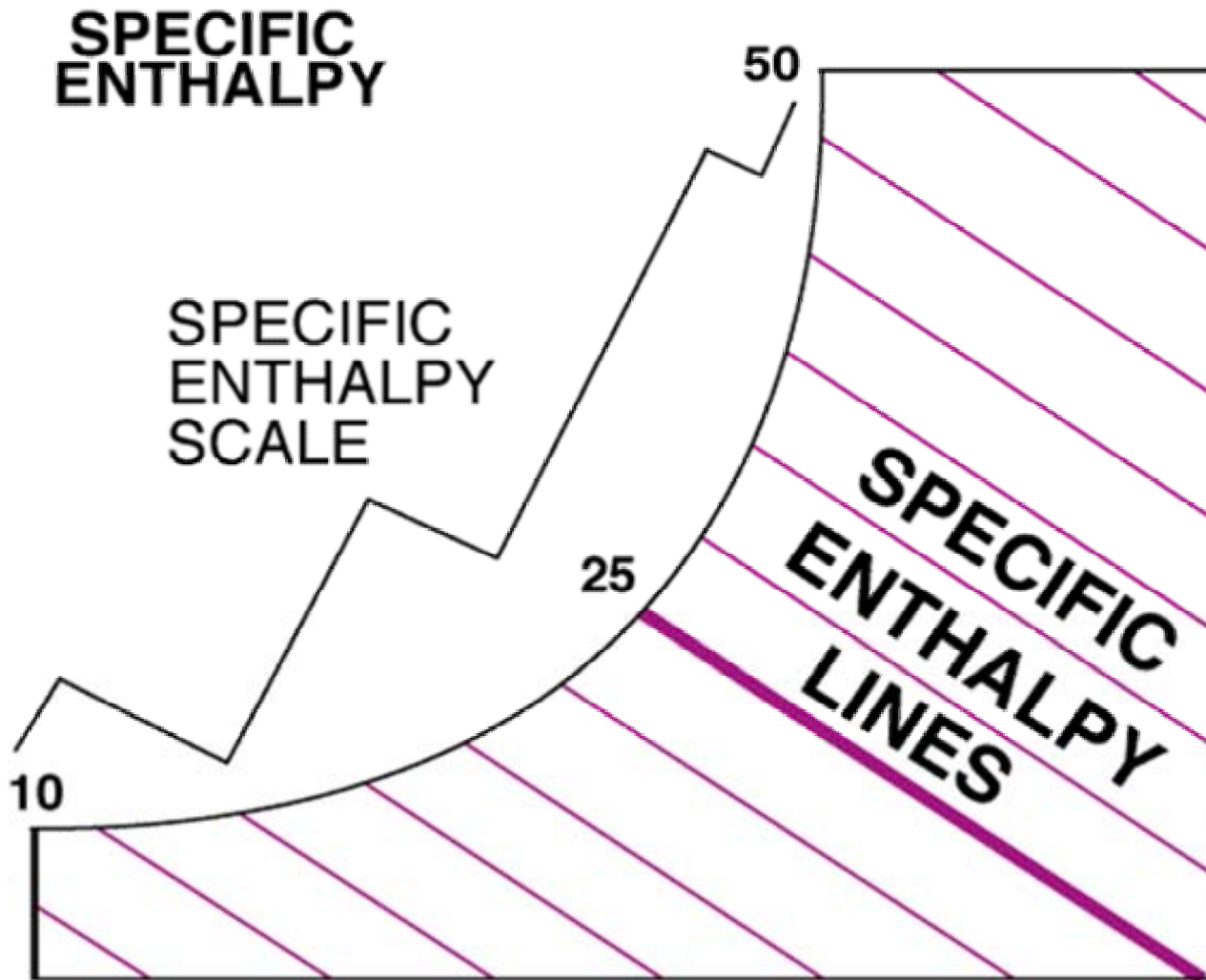
**0.01**

**HUMIDITY  
RATIO**

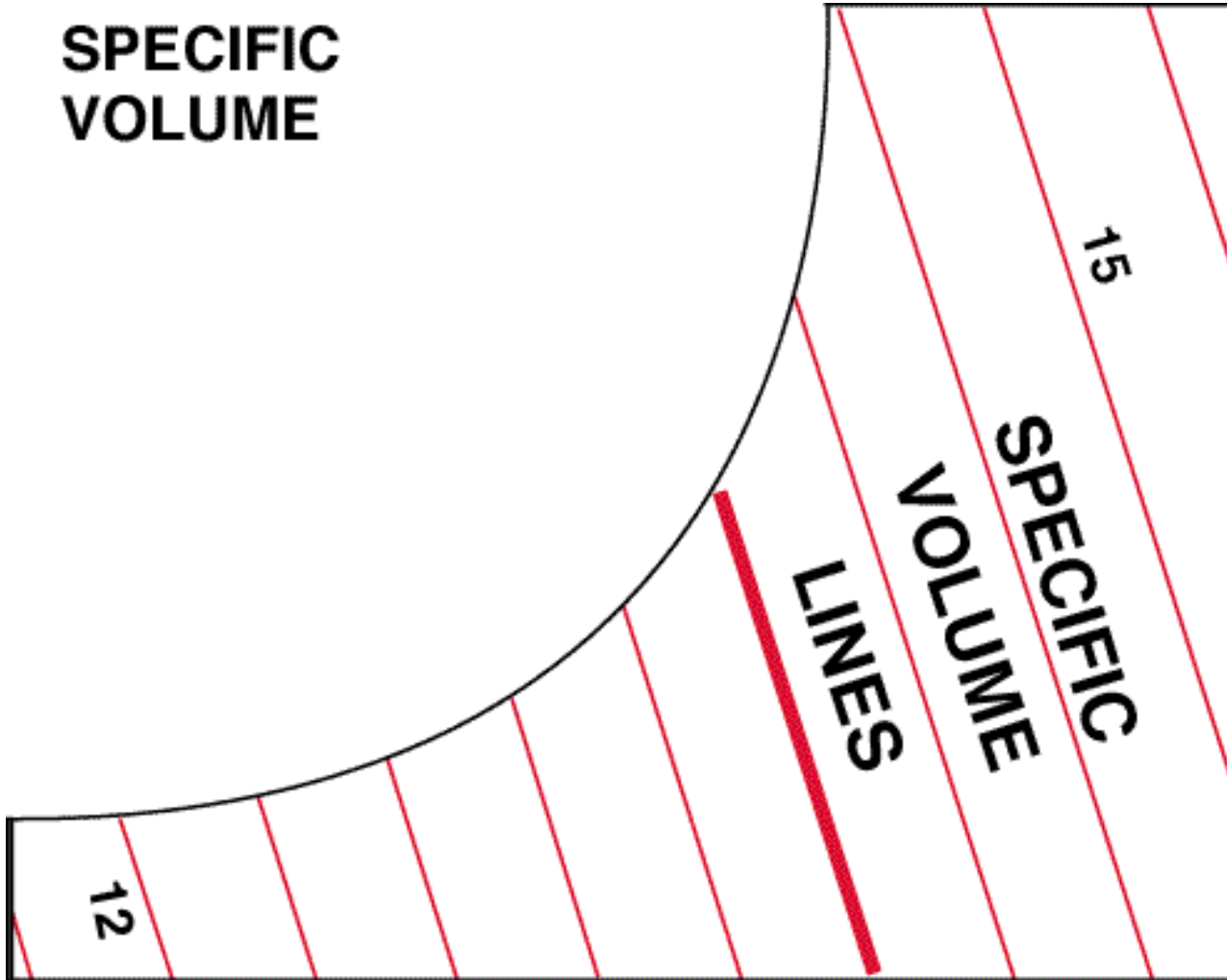
**0**







**SPECIFIC  
VOLUME**



**SPECIFIC  
VOLUME  
LINES**

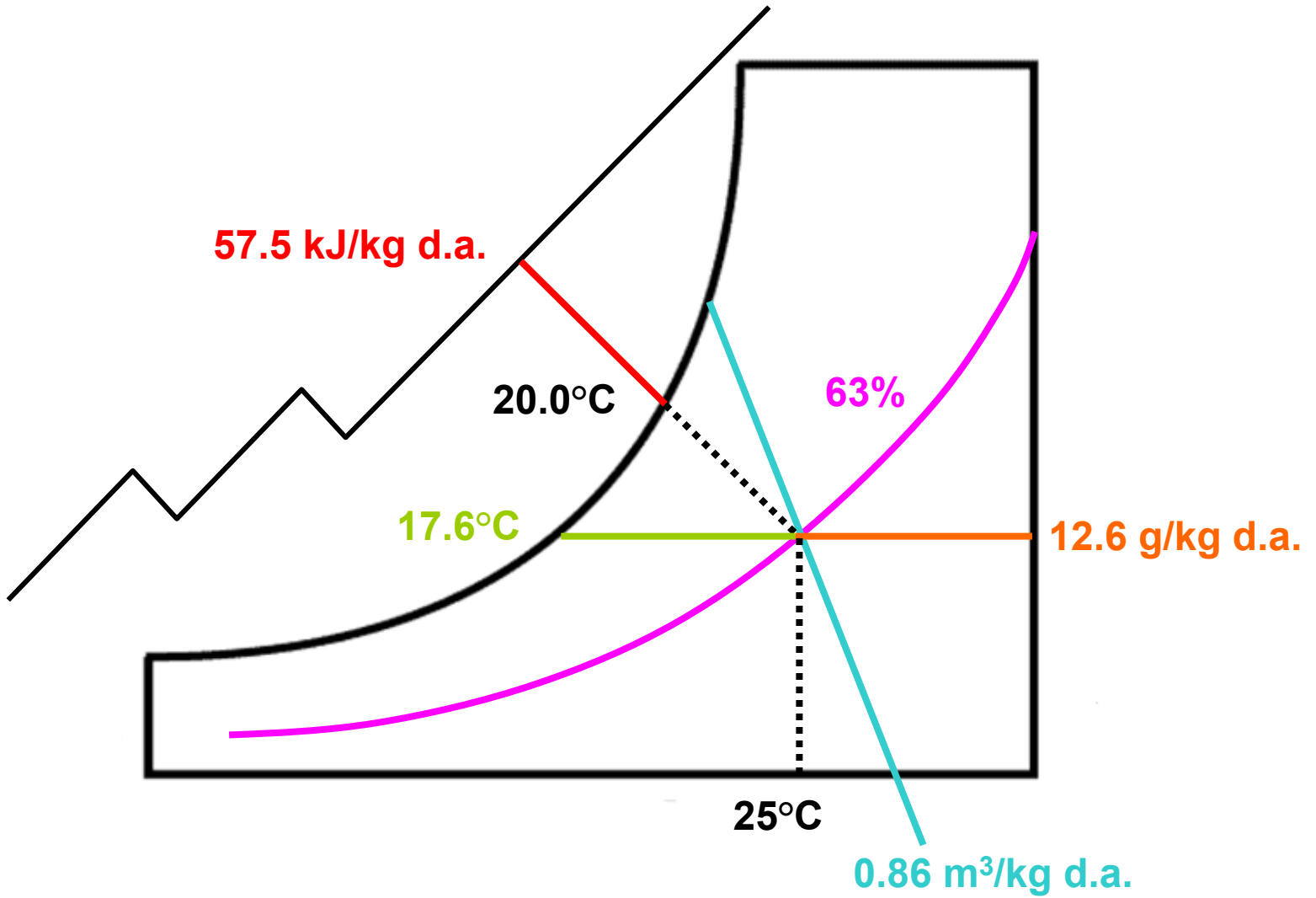
12

15

# Psychrometric chart: Example 1

Given:  $T = 25^{\circ}\text{C}$   
 $T_w = 20^{\circ}\text{C}$

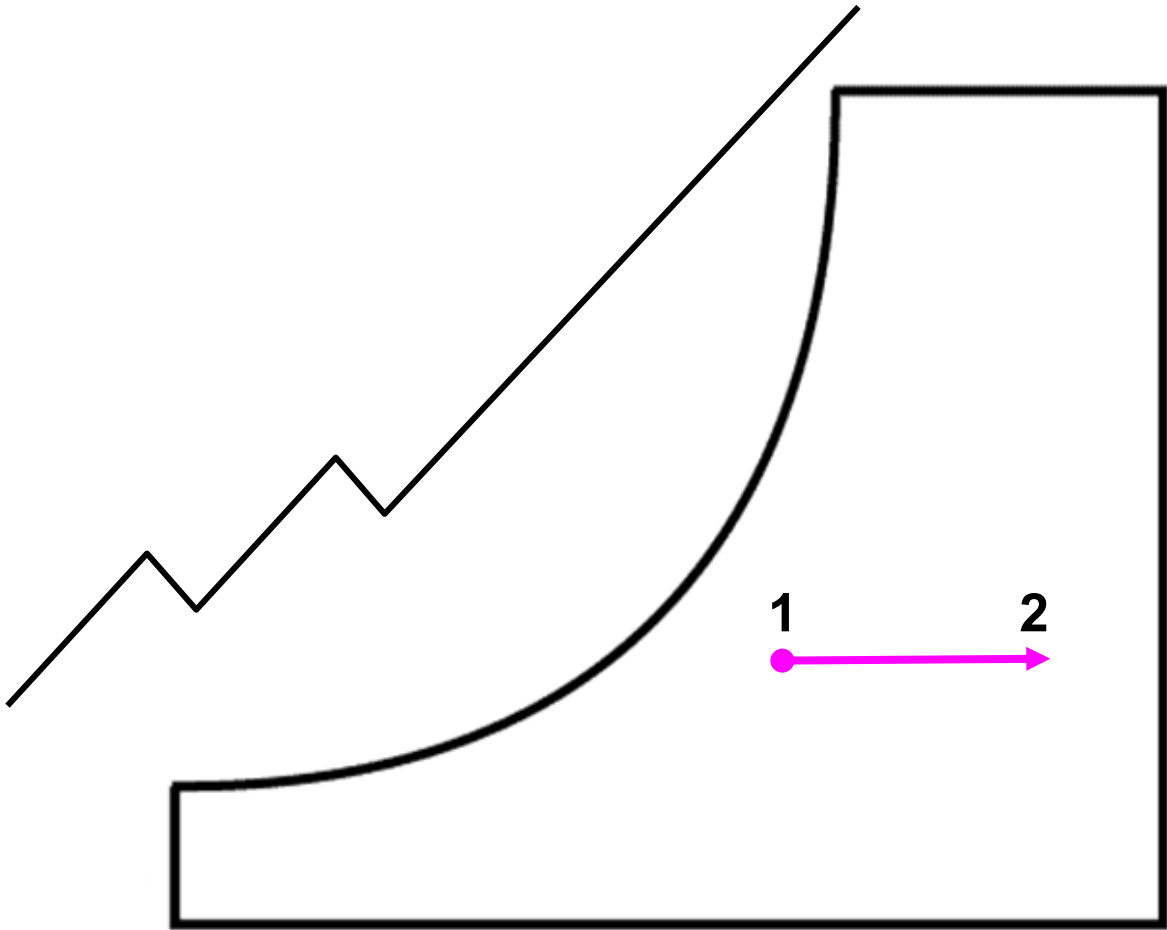
Required: (a) RH, (b)  $T_{dp}$ , (c) HR, (d)  $v$ , (e)  $h$



# PSYCHROMETRIC PROCESSES

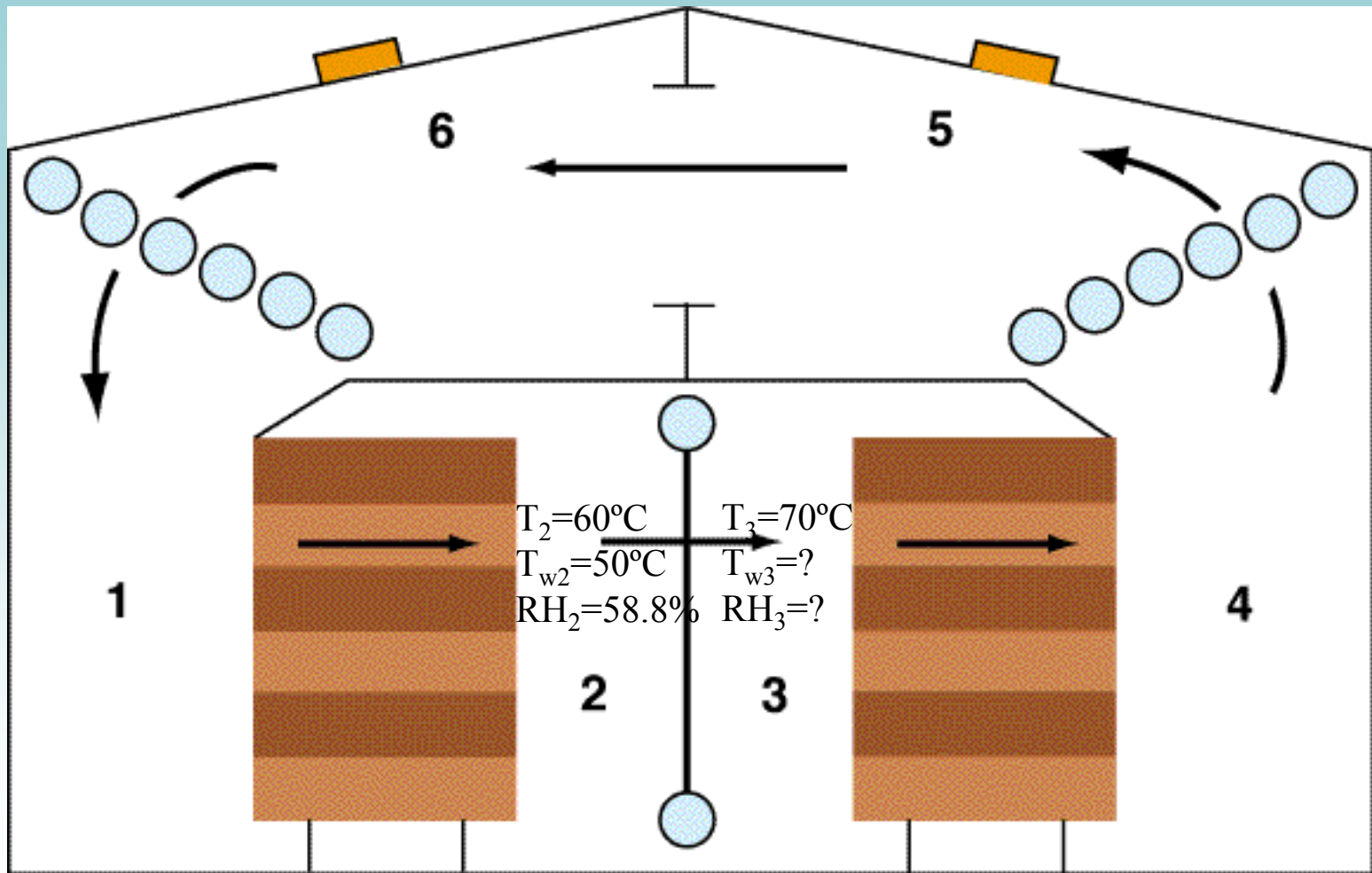
# Sensible Heating or Cooling

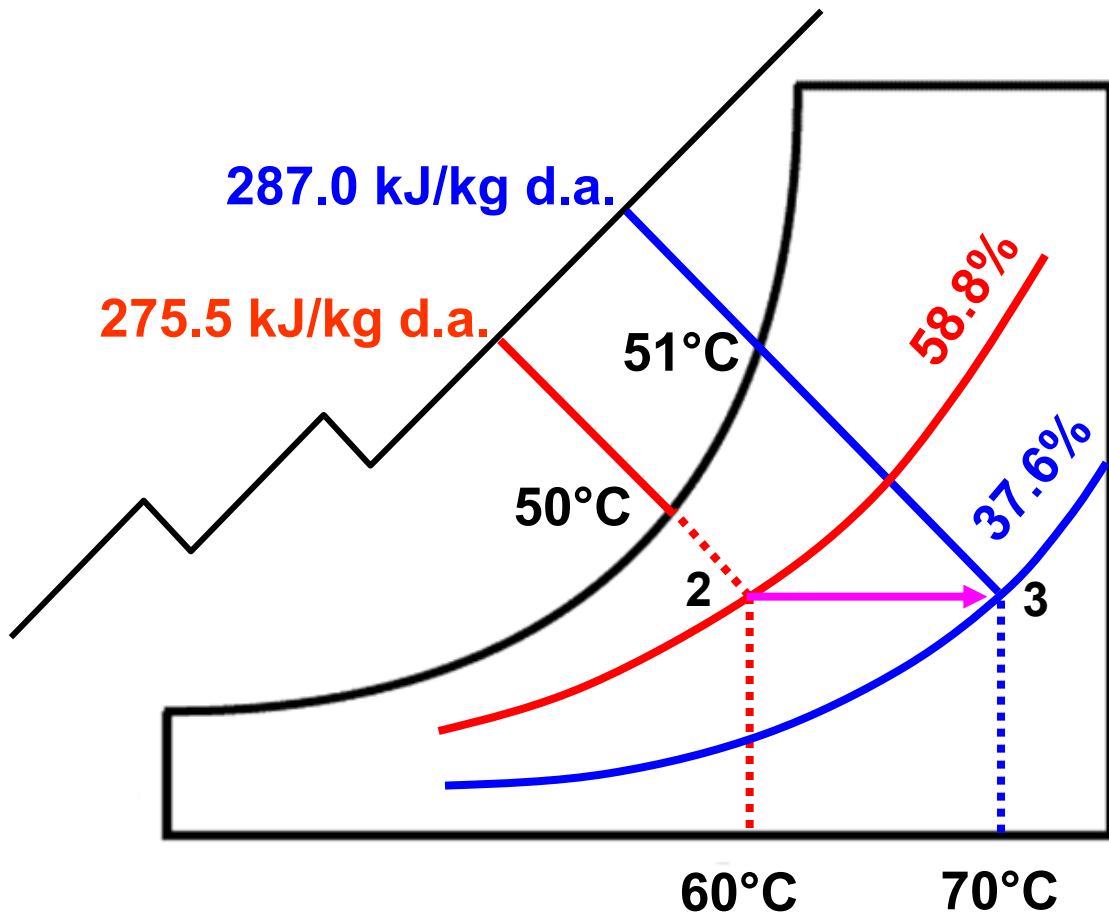
- a psychrometric process that involves the increase or decrease in the temperature of air without changing its humidity ratio
- Example: passing moist air over a room space heater and of kiln air over the heating coils



# Sensible heating: Example 5

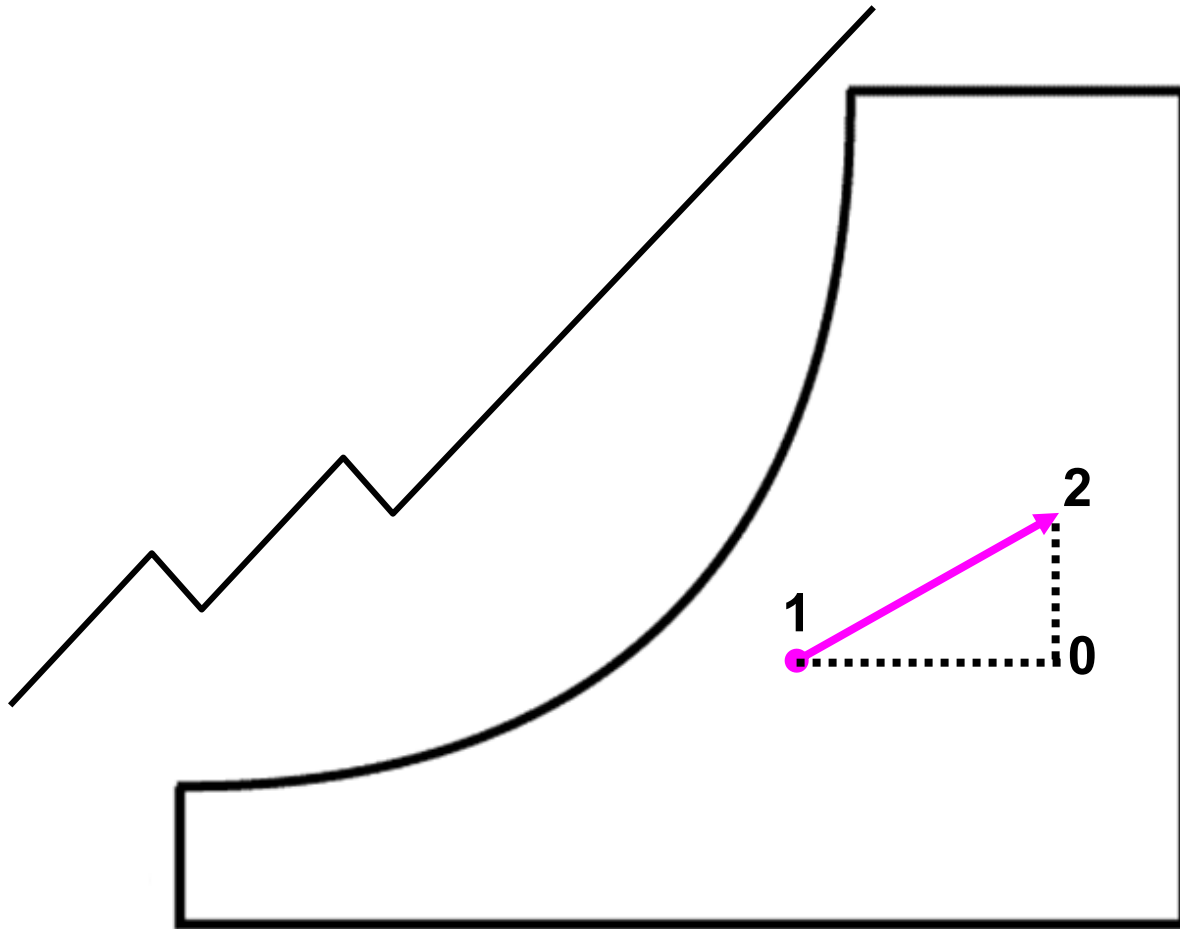






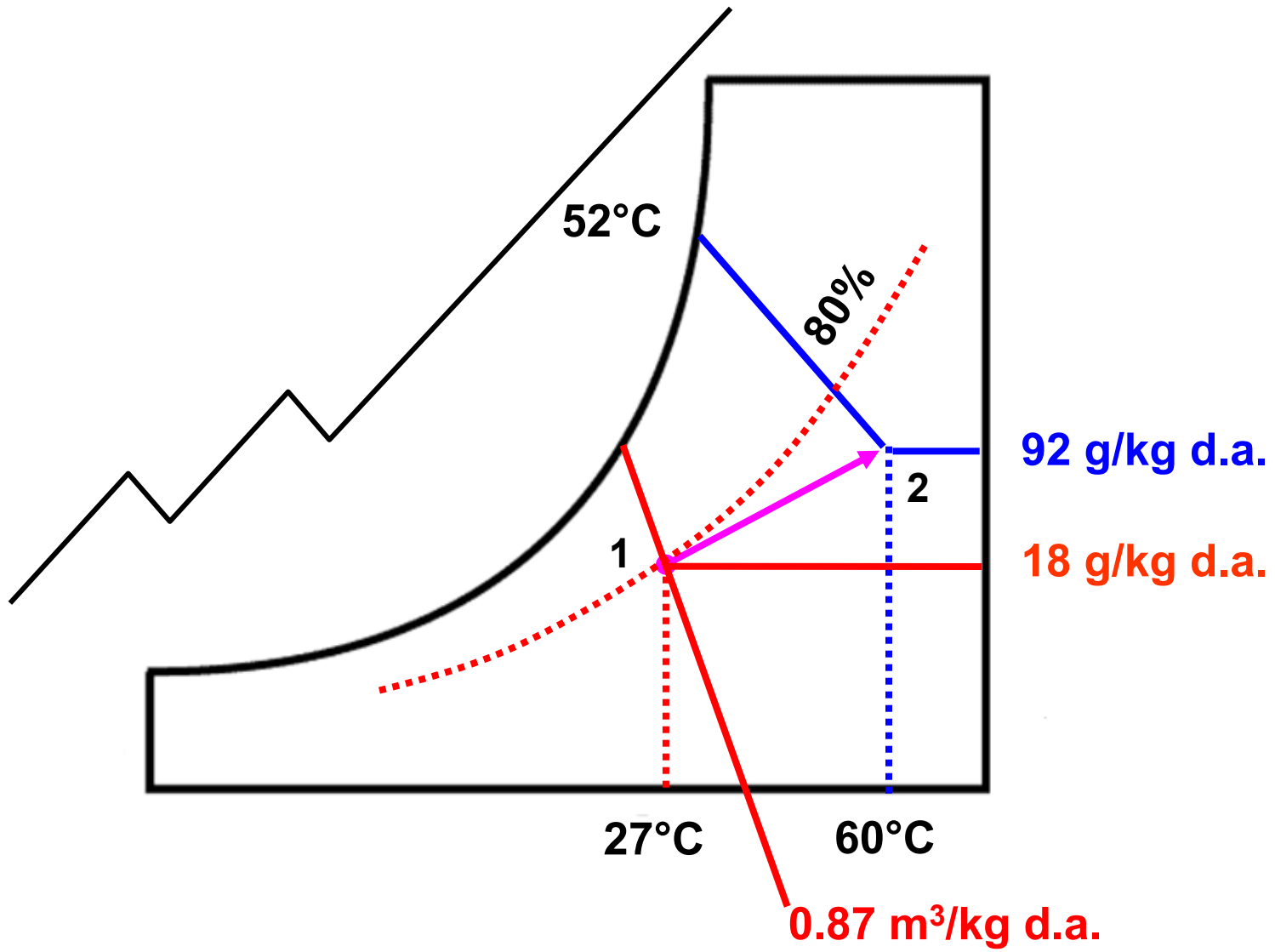
# Heating and Humidifying

- a psychrometric process that involves the simultaneous increase in both the dry bulb temperature and humidity ratio of the air



## Heating and humidifying: Example 7

Two and a half cubic meters of lumber is being dried at  $60^{\circ}\text{C}$  dry bulb temperature and  $52^{\circ}\text{C}$  wet bulb temperature. The drying rate of the lumber is 12.5 kg of water per hour. If outside air is at  $27^{\circ}\text{C}$  dry bulb temperature and 80% relative humidity, how much outside air is needed per minute to carry away the evaporated moisture?



## Heating and humidifying: Example 7

$$\begin{aligned}\Delta HR &= (92.0 - 18.0) \text{ g/kg dry air} \\ &= 74.0 \text{ g/kg dry air}\end{aligned}$$

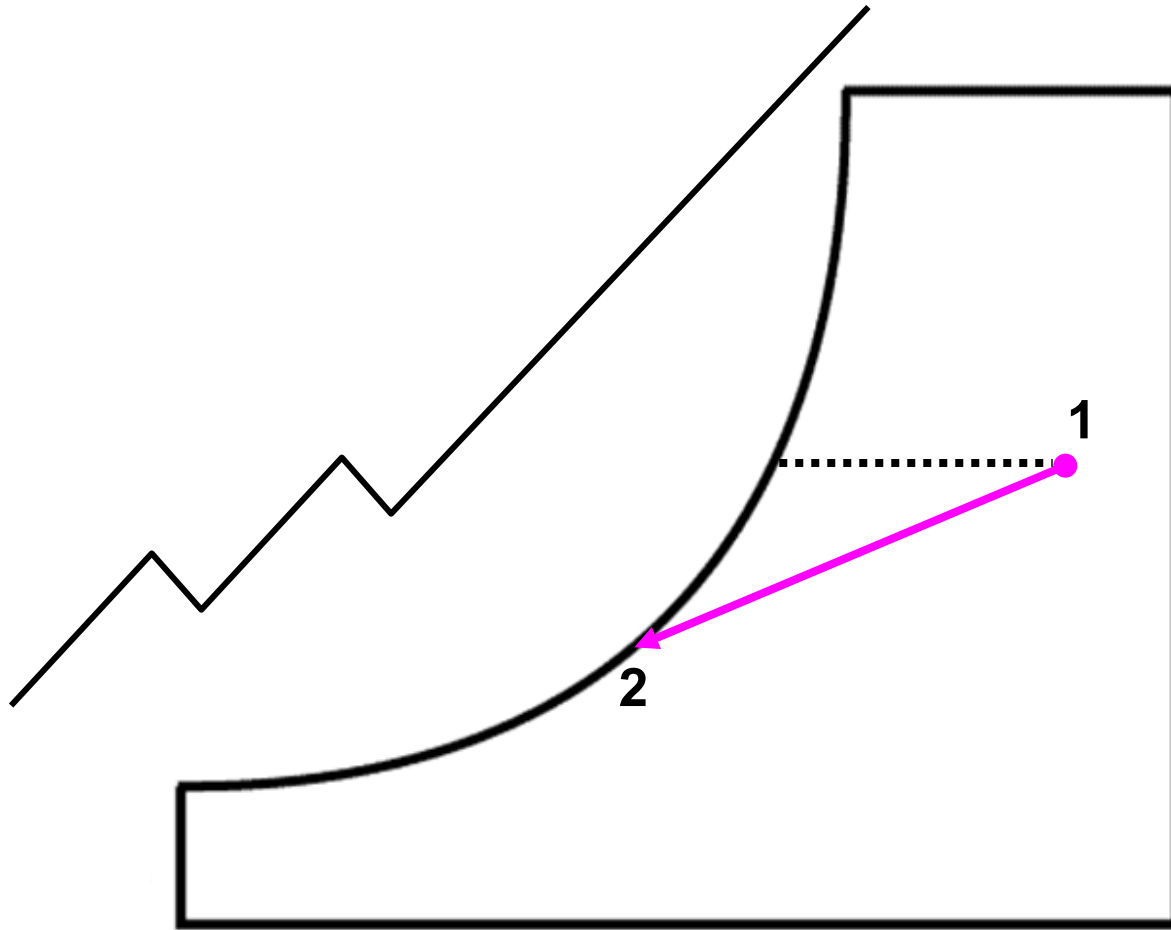
$$\begin{aligned}w_{a1} &= \text{drying rate}/\Delta HR \\ &= (12.5 \text{ kg/hour})/(0.074 \text{ kg/kg dry air}) \\ &= 168.9 \text{ kg dry air/hour}\end{aligned}$$

$$\begin{aligned}VF_1 &= (w_{a1})(v_1) \\ &= (168.9 \text{ kg dry air/hour})(0.87 \text{ m}^3/\text{kg dry air}) \\ &= 147 \text{ m}^3/\text{hour} = 2.45 \text{ m}^3/\text{minute}\end{aligned}$$

# Cooling and Dehumidifying

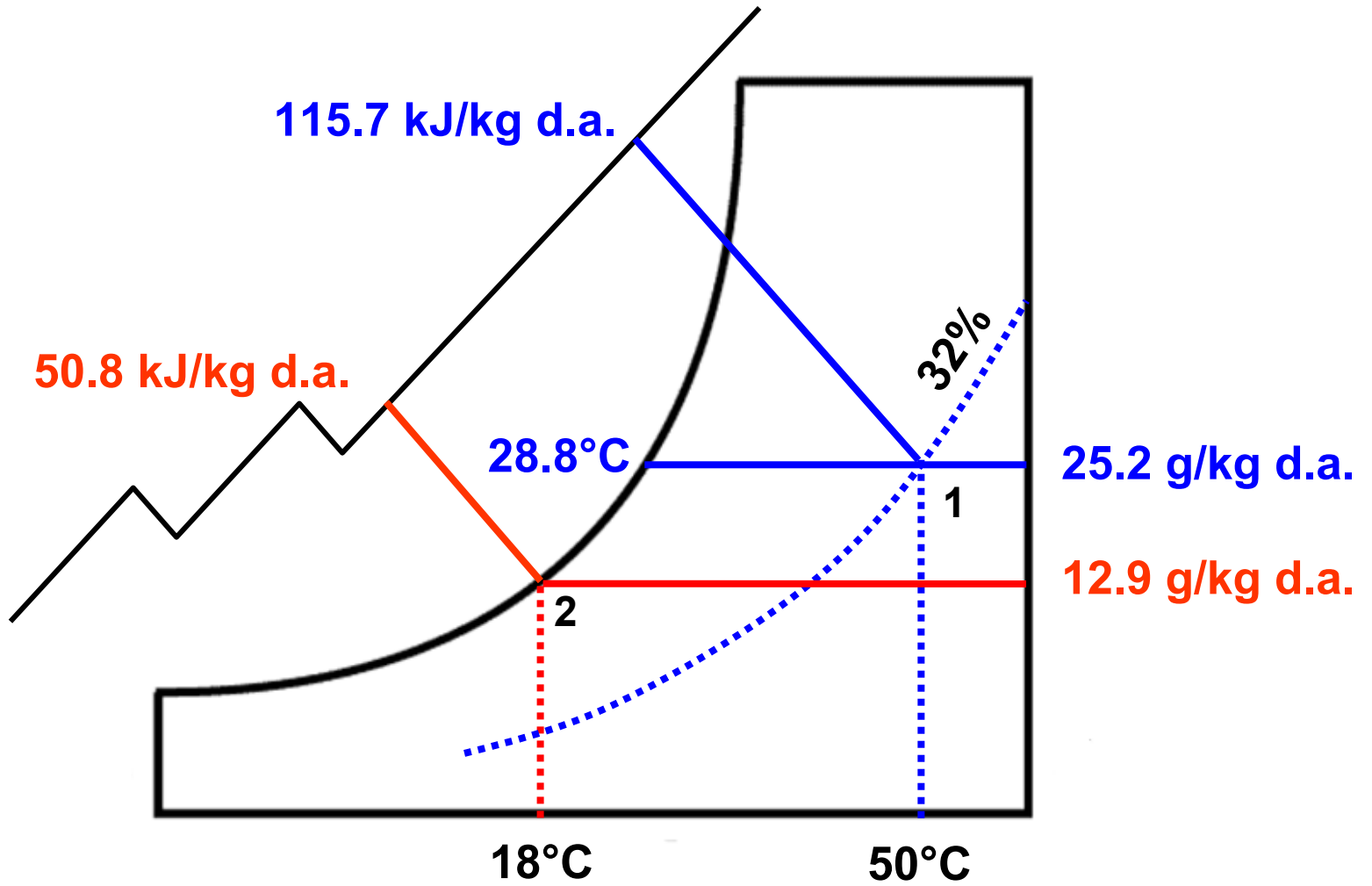
- a psychrometric process that involves the removal of water from the air as the air temperature falls below the dew-point temperature





## Cooling and dehumidifying: Example 9

Moist air at 50°C dry bulb temperature and 32% relative humidity enters the cooling coil of a dehumidification kiln heat pump system and is cooled to a temperature of 18°C. If the drying rate of 6 m<sup>3</sup> of red oak lumber is 4 kg/hour, determine the kW of refrigeration required.



## Cooling and dehumidifying: Example 9

$$\begin{aligned}\Delta HR &= (25.2 - 12.9) \text{ g water/kg dry air} \\ &= 12.3 \text{ g water/kg dry air}\end{aligned}$$

$$\begin{aligned}W_a &= \frac{\text{drying rate}}{\Delta HR} \\ &= \frac{4 \text{ kg water/h}}{0.0123 \text{ kg water/kg dry air}} \\ &= 325.2 \frac{\text{kg dry air}}{\text{h}}\end{aligned}$$

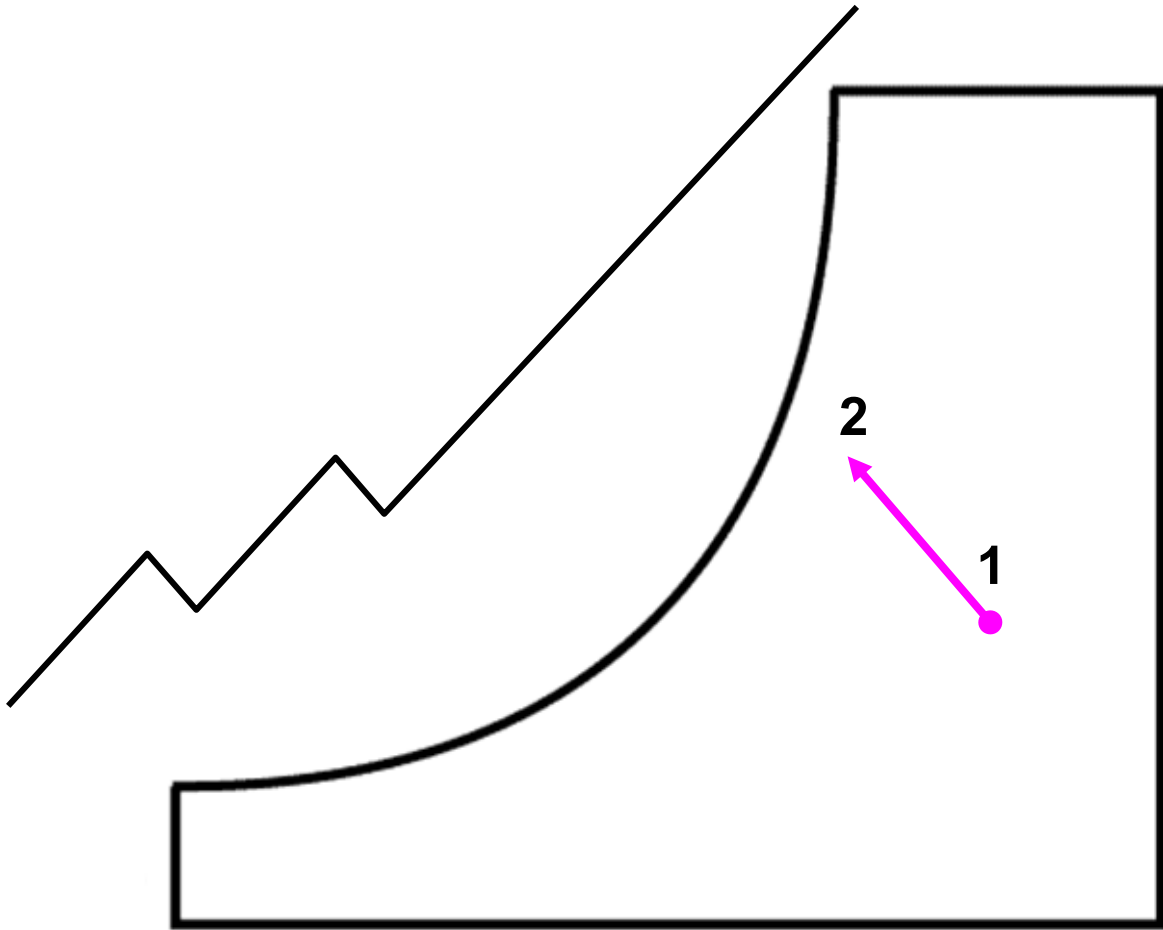
## Cooling and dehumidifying: Example 9

$$\begin{aligned}\Delta h &= (115.7 - 50.8) \text{ kJ/kg dry air} \\ &= 64.9 \text{ kJ/kg dry air}\end{aligned}$$

$$\begin{aligned}q &= (\Delta h)(w_a) \\ &= \left[ 64.9 \frac{\text{kJ}}{\text{kg dry air}} \right] \left[ 325.2 \frac{\text{kg dry air}}{\text{h}} \right] \\ &= 21105.7 \frac{\text{kJ}}{\text{h}} = 5.9 \text{ kW}\end{aligned}$$

# Adiabatic or Evaporative Cooling

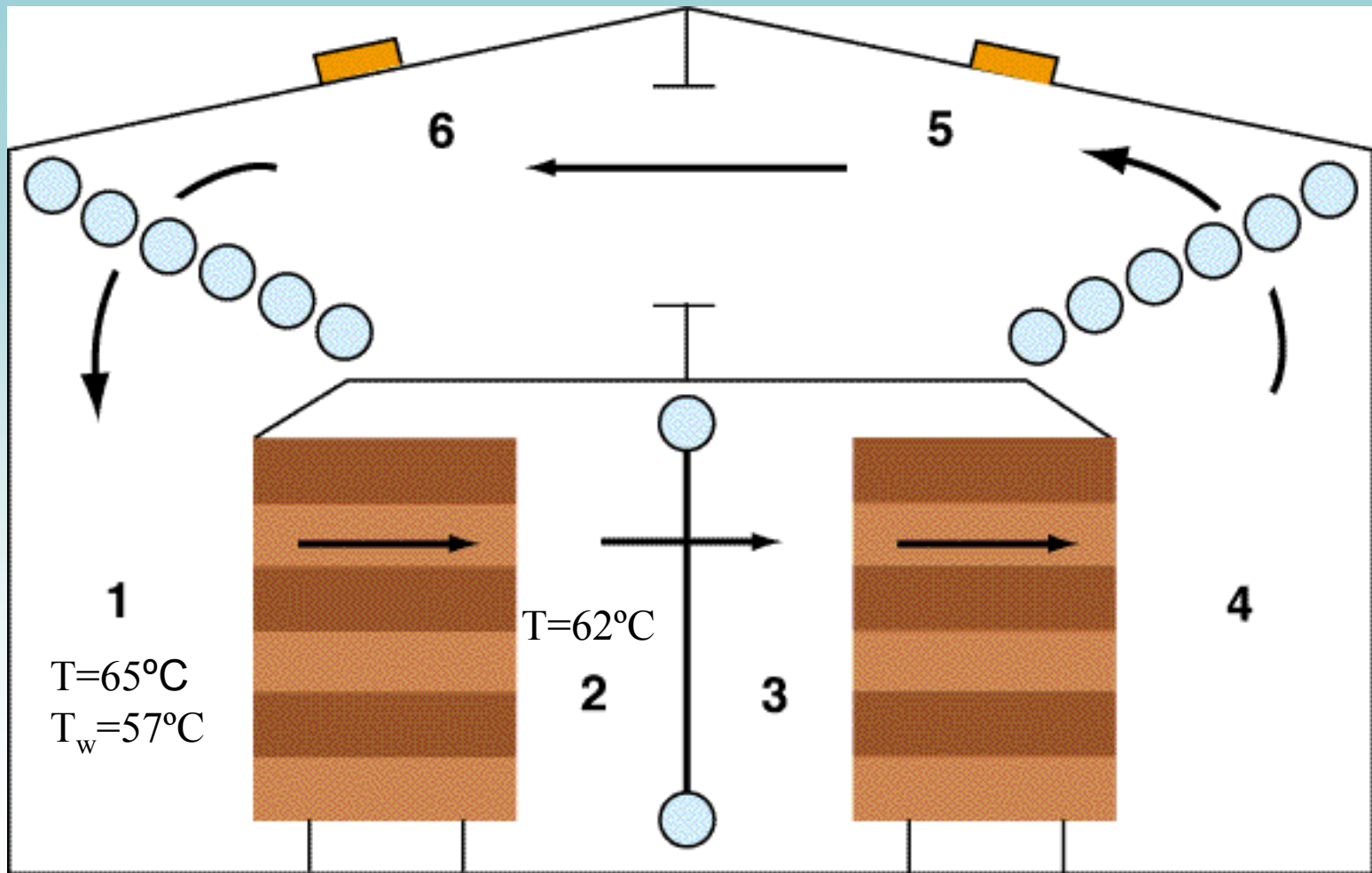
- a psychrometric process that involves the cooling of air without heat loss or gain. Sensible heat lost by the air is converted to latent heat in the added water vapor



## Evaporative cooling: Example 10

Referring to Figure 21, air at state point 1 ( $65^{\circ}\text{C}$  dry bulb temperature and  $57^{\circ}\text{C}$  wet bulb temperature) experiences a temperature drop of  $3^{\circ}\text{C}$  as it passes through the 1.2-m wide stack of lumber. Determine the properties of the air at state point 2 and compare them with those at state point 1. If the air is flowing at a rate of 2 meters per second, determine the drying rate assuming that the volume of the stack of 2.5-cm-thick lumber is  $2.5\text{ m}^3$ . The stack is 1.2 m wide x 3.6 m long, and the boards are separated by stickers 3.8 cm wide x 1.9 cm thick that are spaced 0.6 m apart.





## Evaporative cooling: Example 10

Given:  $T_1 = 65^\circ\text{C}$ ;  $T_{w1} = 57^\circ\text{C}$

Adiabatic cooling to  $T_2 = 62^\circ\text{C}$

Air flow rate = 2 m/s

Volume of lumber = 2.5 m<sup>3</sup>

Board thickness = 2.5 cm

Stack dimensions: 1.2 m wide x 3.6 m long

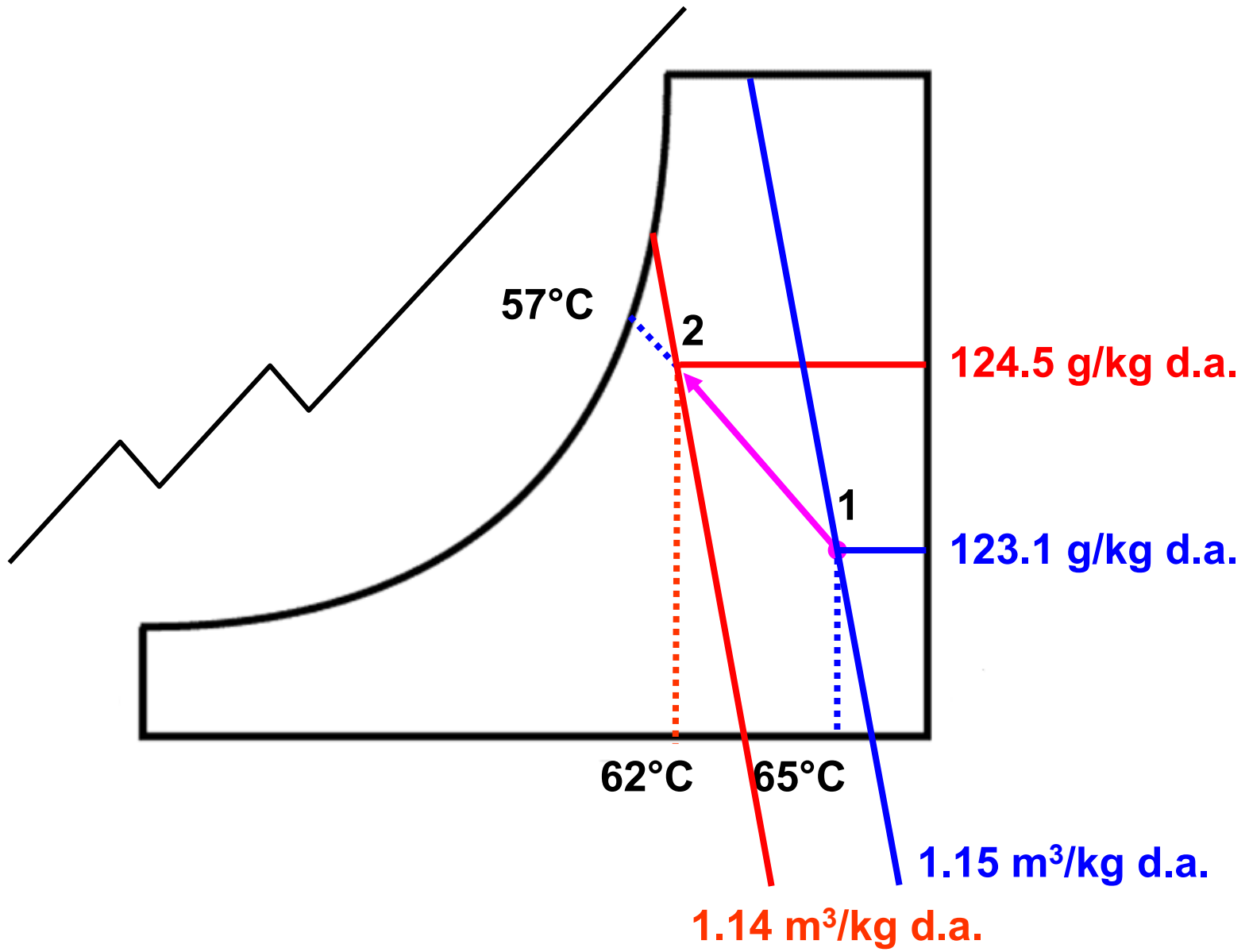
Sticker dimensions: 3.8 cm wide x 1.9 cm thick

Sticker spacing = 0.6 m

Required: (a) Properties of the air at state point 2  
relative to that at state point 1

(b) Drying rate

Solution:



# Evaporative cooling: Example 10

(a) At state point 1:  $T_1 = 65^\circ\text{C}$

$$T_{w1} = 57^\circ\text{C}$$

$$T_{dp1} = 56.3^\circ\text{C}$$

$$RH_1 = 66.9\%$$

$$HR_1 = 123.1 \text{ g/kg of dry air}$$

$$v_1 = 1.15 \text{ m}^3/\text{kg of dry air}$$

$$h_1 = 387.7 \text{ kJ/kg of dry air}$$

At state point 2:  $T_2 = 62^\circ\text{C}$

$$T_{w2} = 57^\circ\text{C}$$

$$T_{dp2} = 56.5^\circ\text{C}$$

$$RH_2 = 77.3\%$$

$$HR_2 = 124.5 \text{ g/kg of dry air}$$

$$v_2 = 1.14 \text{ m}^3/\text{kg of dry air}$$

$$h_2 = 387.7 \text{ kJ/kg of dry air}$$

## Evaporative cooling: Example 10

$$(b) \quad \text{Drying rate} = (\Delta HR)(w_a)$$

$$w_a = \frac{VF}{V_2}$$

$$VF = (A)(\text{air flow rate})$$

## Evaporative cooling: Example 10

$$A = \left( \frac{V}{P_1 P_w B_t} \right) \left( P_1 S_t - \frac{P_1 + S_s}{S_s} S_t S_w \right)$$

$$A = \left( \frac{2.5}{3.6 * 1.2 * 0.025} \right) \left( 3.6 * 0.019 - \frac{3.6 + 0.6}{0.6} 0.019 * 0.038 \right)$$

$$A = 1.47 \text{ m}^2$$

## Evaporative cooling: Example 10

$$A = 1.47 \text{ m}^2$$

$$VF = (A)(\text{air flow rate})$$

$$VF = \left(1.47 \text{ m}^2\right) \left(2 \frac{\text{m}}{\text{s}}\right) = 2.9 \frac{\text{m}^3}{\text{s}}$$

## Evaporative cooling: Example 10

$$VF = 2.9 \frac{\text{m}^3}{\text{s}}$$

$$W_a = \frac{VF}{V_2}$$

$$W_a = \frac{2.9 \frac{\text{m}^3}{\text{s}}}{1.14 \frac{\text{m}^3}{\text{kg dry air}}} = 2.6 \frac{\text{kg dry air}}{\text{s}}$$



## Evaporative cooling: Example 10

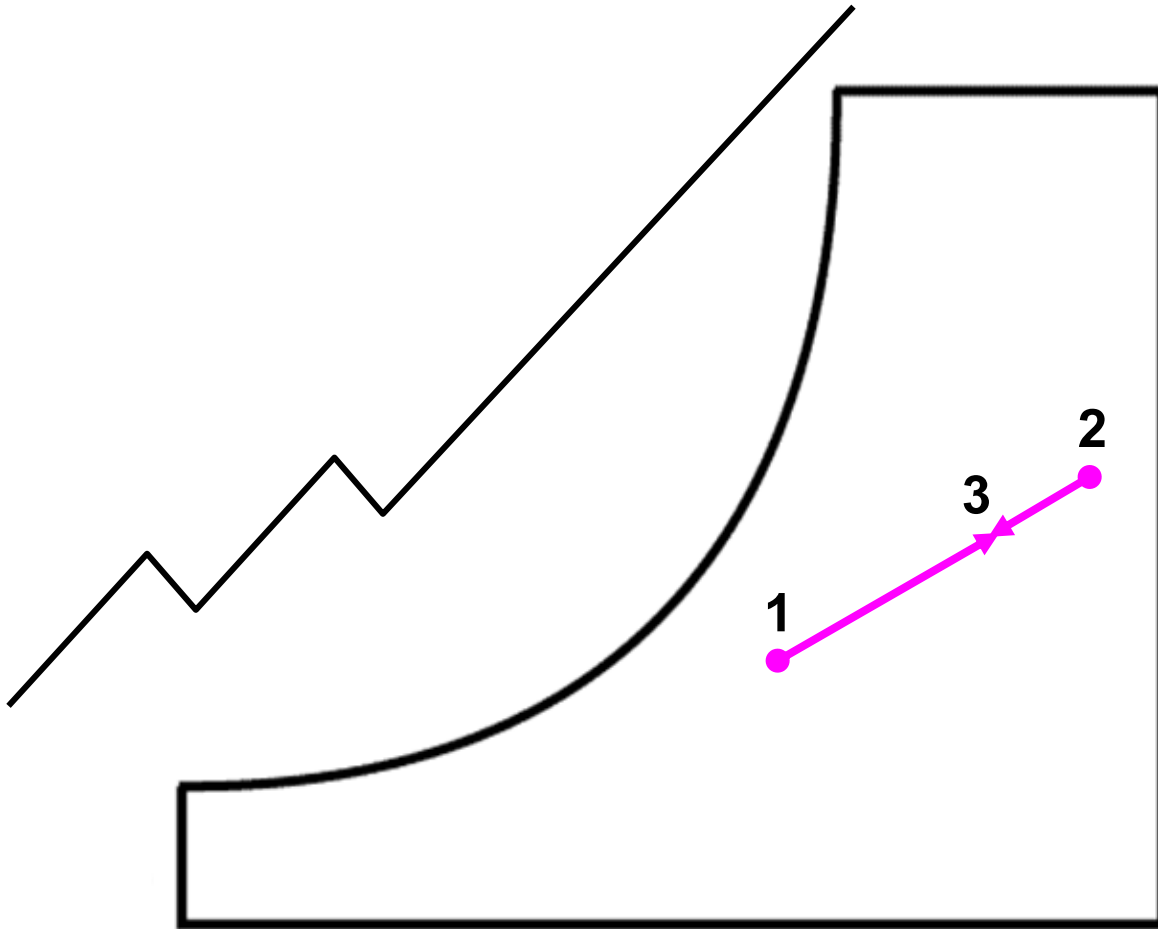
$$w_a = 2.6 \frac{\text{kg dry air}}{\text{s}}$$

$$\text{Drying rate} = (w_a)(\Delta HR)$$

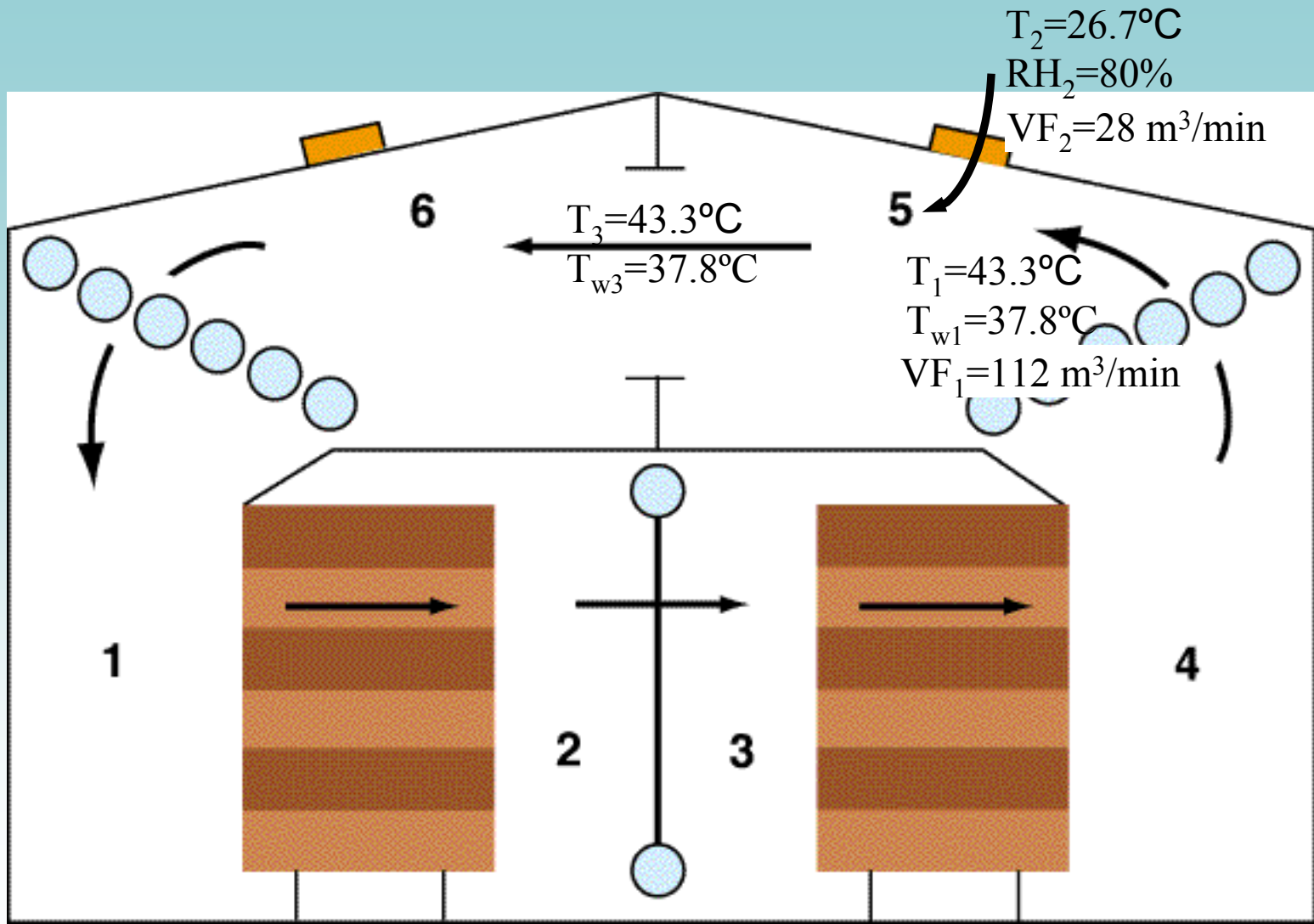
$$\begin{aligned} \text{Drying rate} &= \left( 2.6 \frac{\text{kg dry air}}{\text{s}} \right) \left( 1.4 \frac{\text{g}}{\text{kg dry air}} \right) \\ &= 3.6 \frac{\text{g}}{\text{s}} = 13.0 \frac{\text{kg}}{\text{h}} \end{aligned}$$

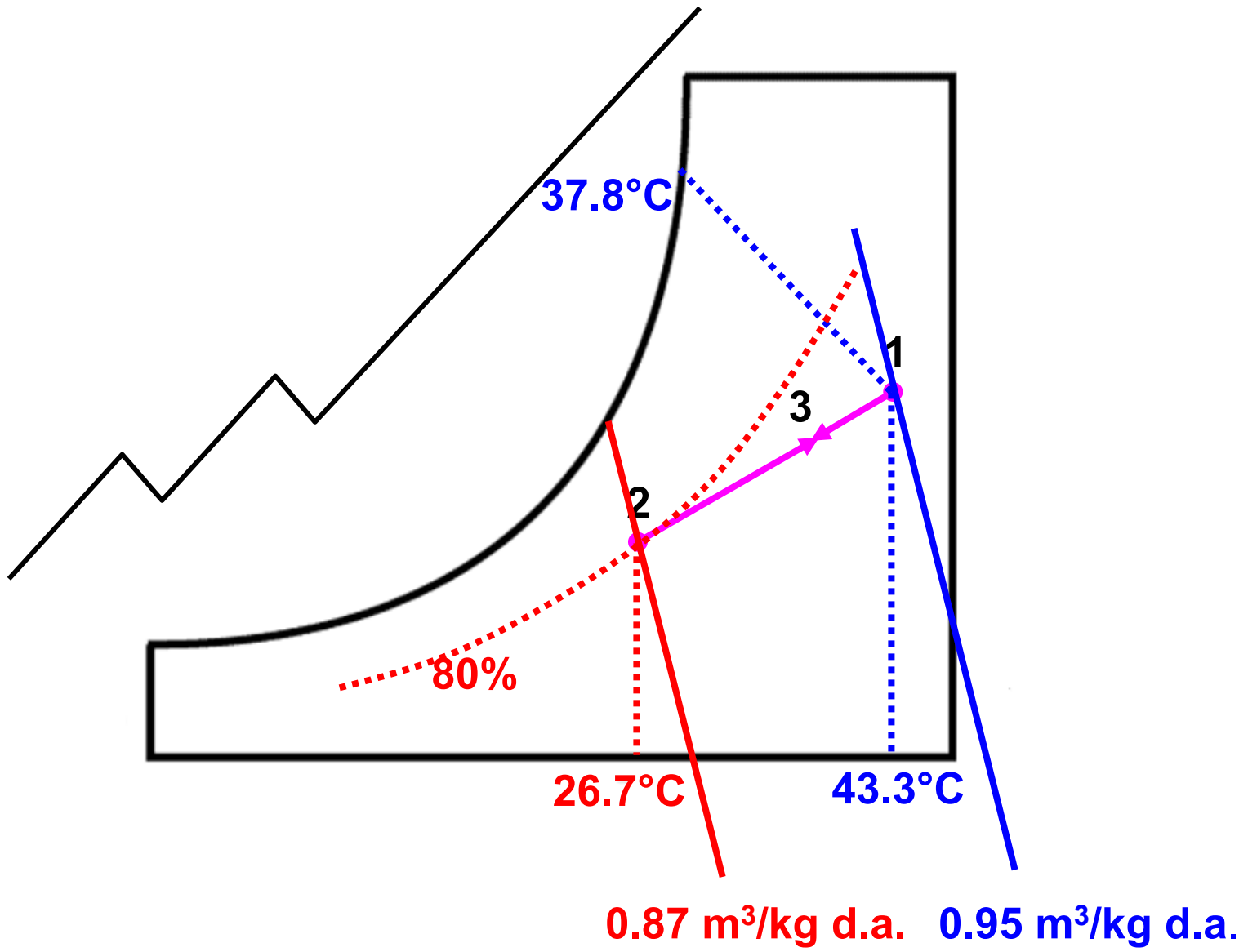
# Adiabatic Mixing of Moist Air Stream

- A psychrometric process that involves no net heat loss or gain during the mixing of two air streams



# Adiabatic mixing: Example 11





## Adiabatic mixing: Example 11

$$W_a = \frac{VF}{v}$$

$$W_{a1} = \frac{112 \frac{\text{m}^3}{\text{minute}}}{0.95 \frac{\text{m}^3}{\text{kg dry air}}} = 117.9 \frac{\text{kg dry air}}{\text{minute}}$$

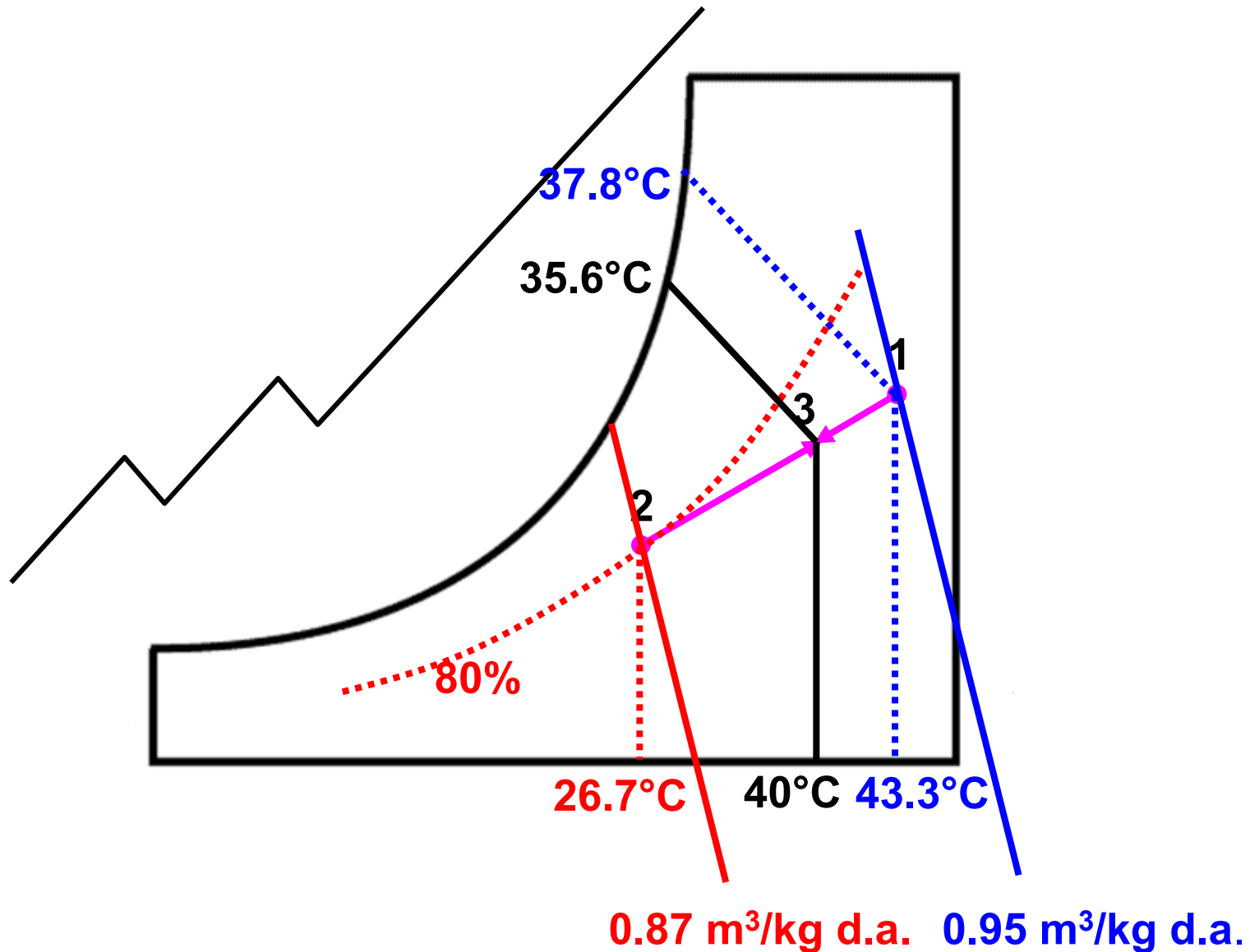
$$W_{a2} = \frac{28 \frac{\text{m}^3}{\text{minute}}}{0.87 \frac{\text{m}^3}{\text{kg dry air}}} = 32.2 \frac{\text{kg dry air}}{\text{minute}}$$

## Adiabatic mixing: Example 11

$$\frac{\text{line 1-3}}{\text{line 1-2}} = \frac{w_{a2}}{w_{a2} + w_{a1}} = \frac{32.2}{32.2 + 117.9} = 0.21$$

Therefore, length of line segment 1-3 is 0.21 times the length of line 1-2





# Adiabatic mixing: Example 11

$$T_3 = 40.0^\circ\text{C}$$

$$T_{w3} = 35.6^\circ\text{C}$$